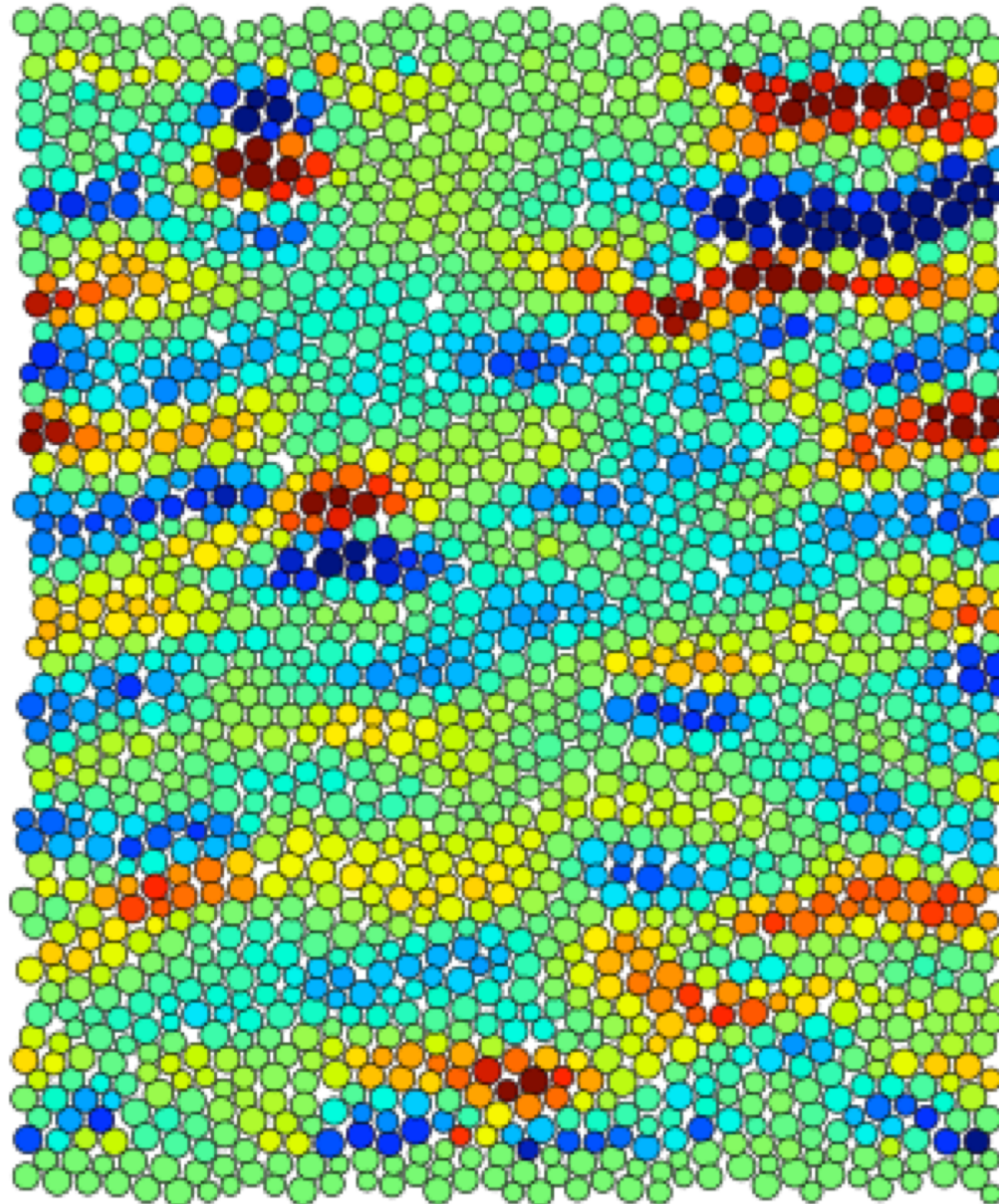


Rheology and jamming of granular systems and suspensions

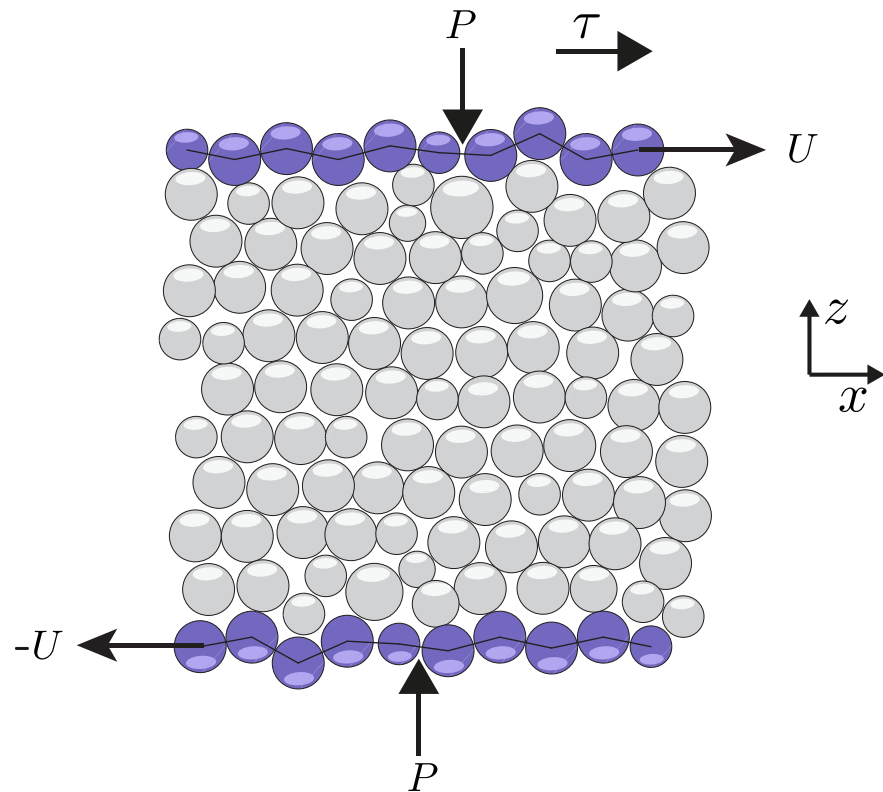


B. Andreotti
M. Bouzid
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Philippe Claudin



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Homogeneous shear flow of rigid particles



Inertial number

$$I = \frac{\dot{\gamma}d}{\sqrt{P/\rho}}$$

effective friction

$$\mu = \frac{\tau}{P}$$

volumic fraction

$$\phi$$

coordination number

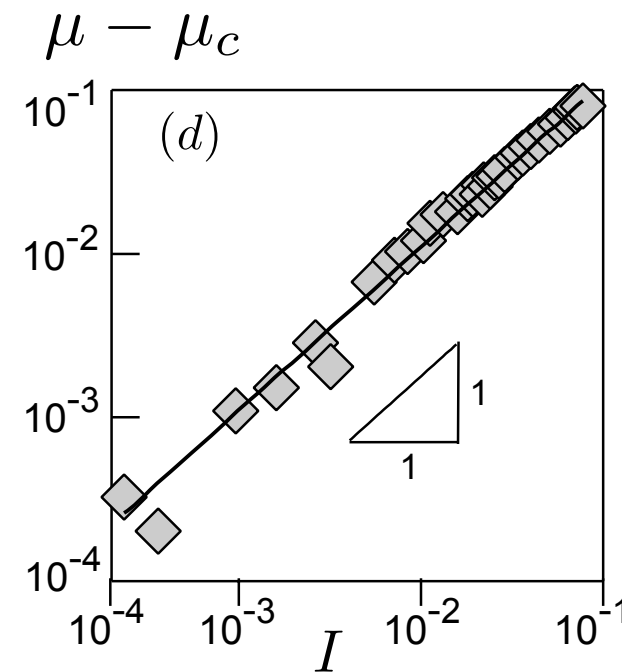
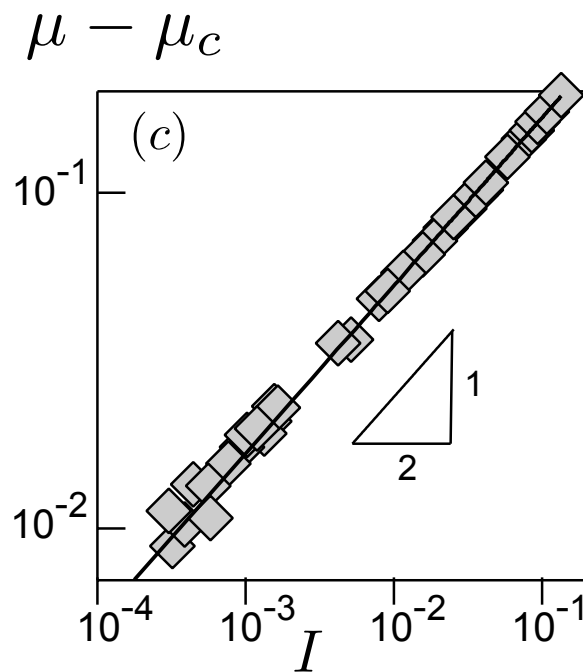
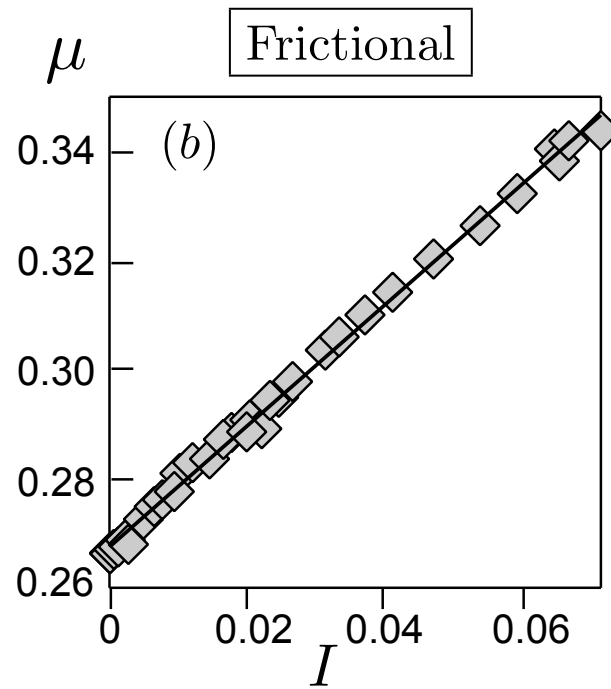
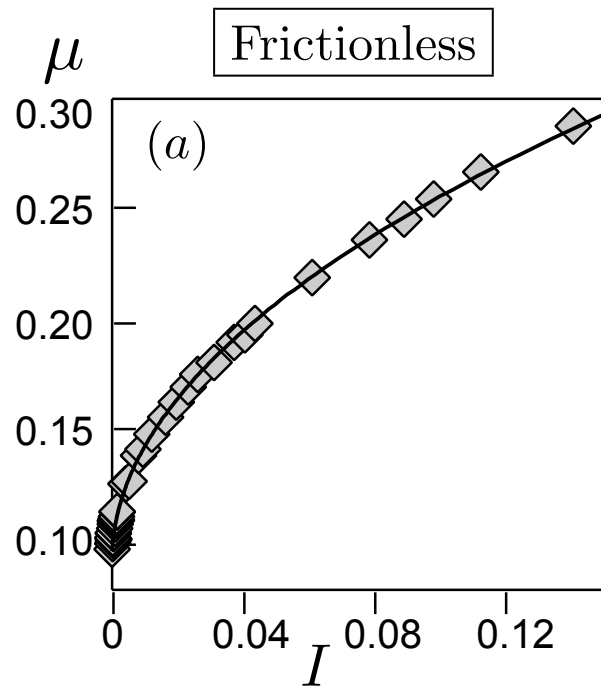
$$Z$$

GdR MiDi, EPJE **14**, 341 (2004).

da Cruz et al., PRE **72**, 021309 (2005).

Jop et al., Nature **441**, 727 (2006).

Local rheology

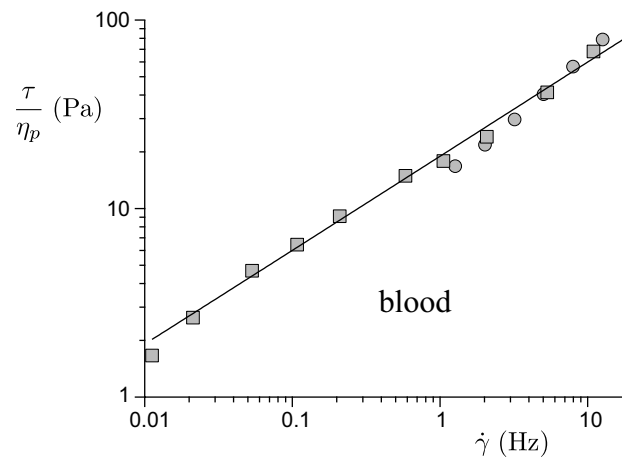
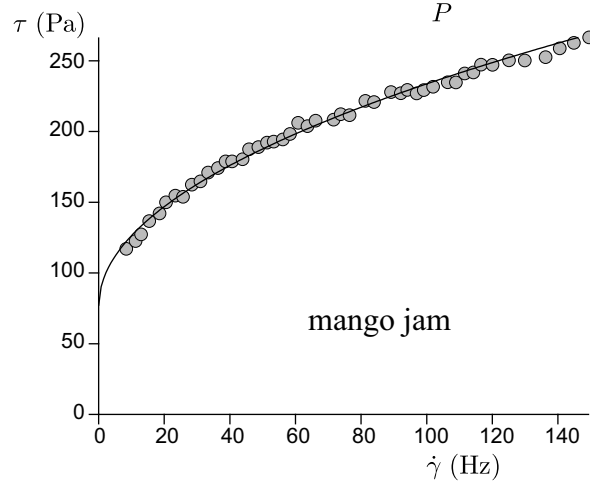
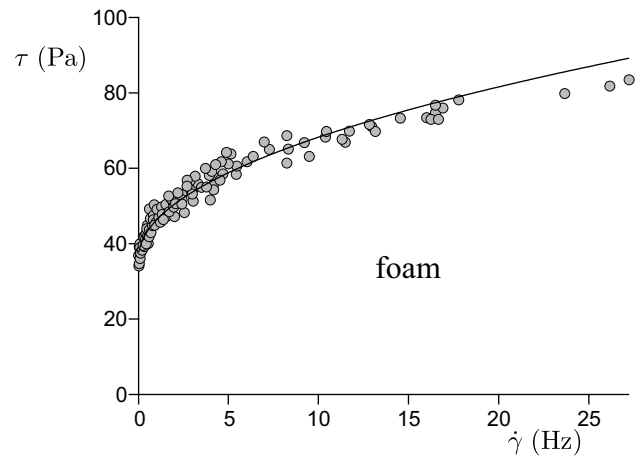
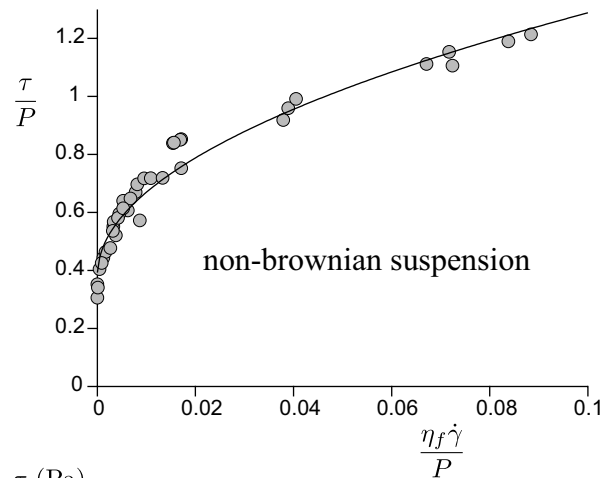
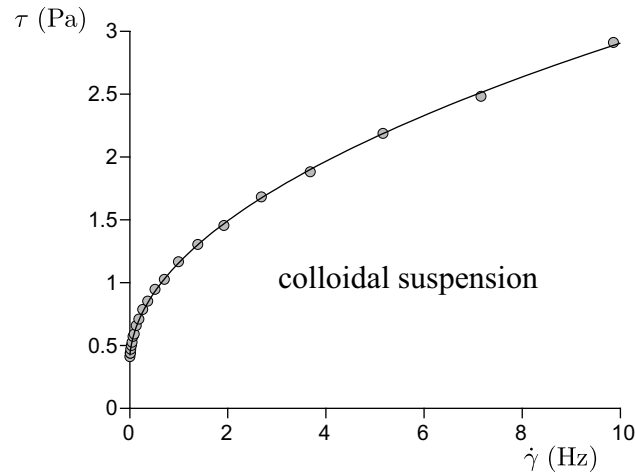
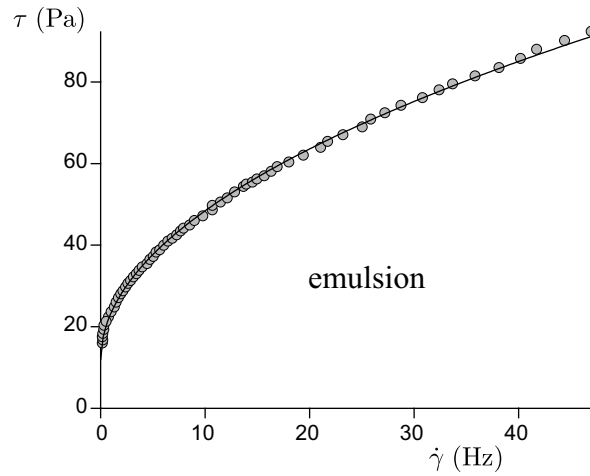


$$\mu = \mu_c + aI^\alpha$$

$$\phi = \phi_c - bI^\alpha$$

$$\gamma = \frac{\mu}{\mu_c}$$

Rheologies of amorphous materials



Goyon et al., Nature **454**, 84 (2008).

Willenbacher et al., Soft Matter **7**, 5777 (2011).

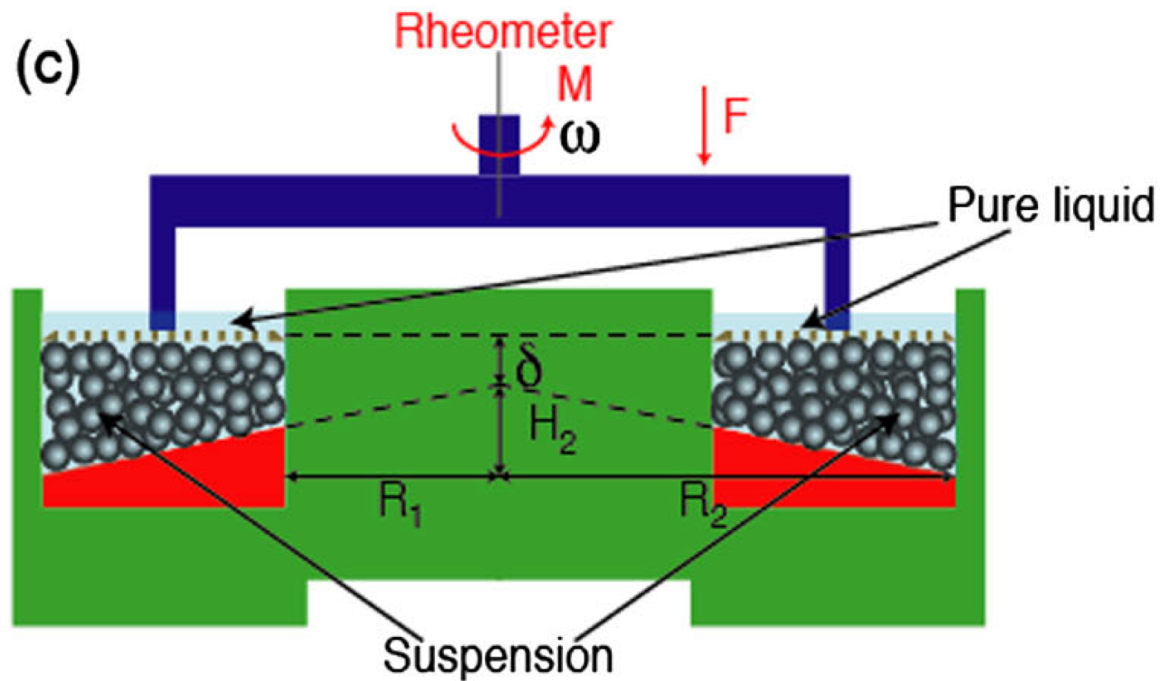
Boyer et al., PRL **107**, 188301 (2011).

Ovarlez et al., EPL **91**, 68005 (2010).

Basu & Shivhare, J. Food. Eng. **100**, 357 (2010).

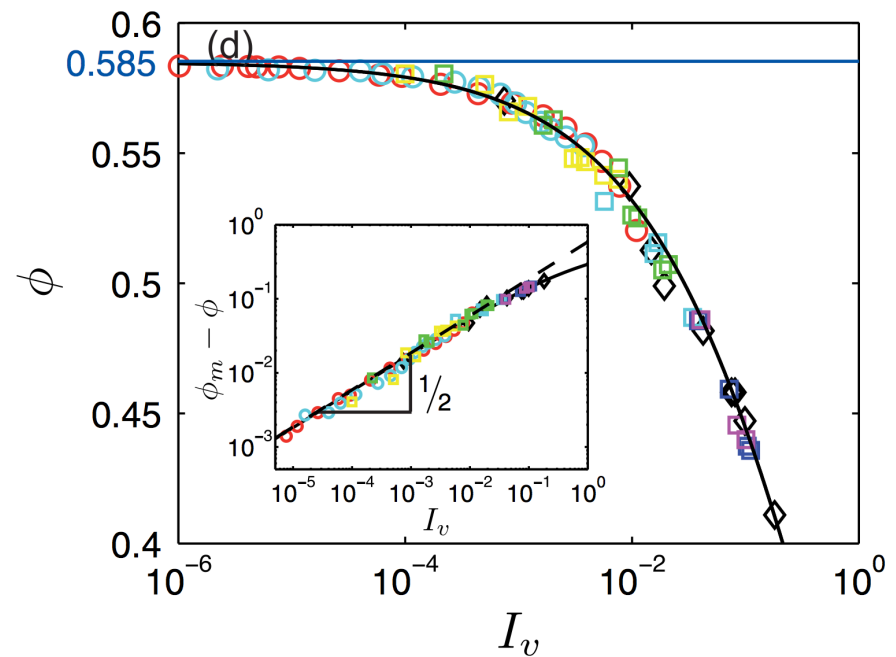
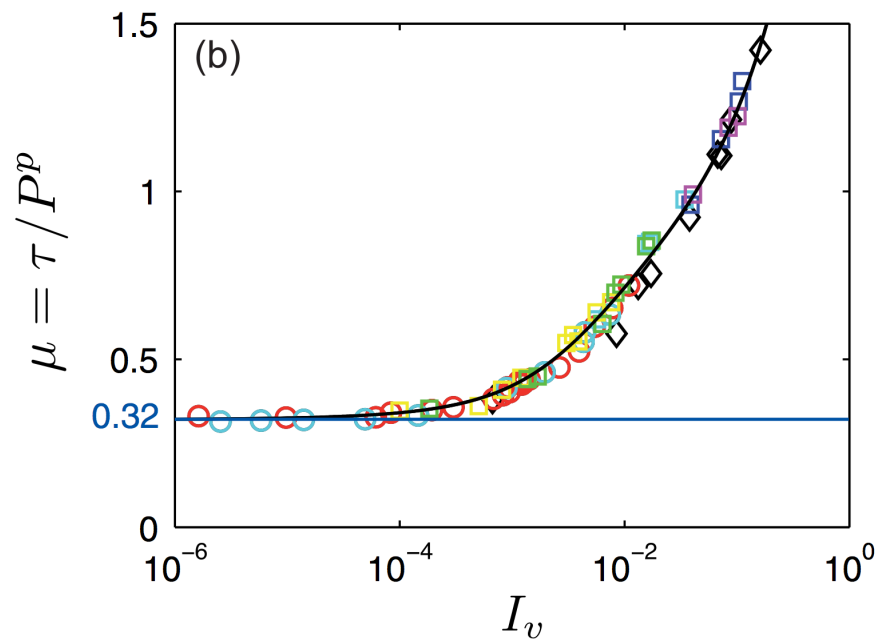
Chien Science **168**, 977(1970).

Rheology of dense granular suspensions

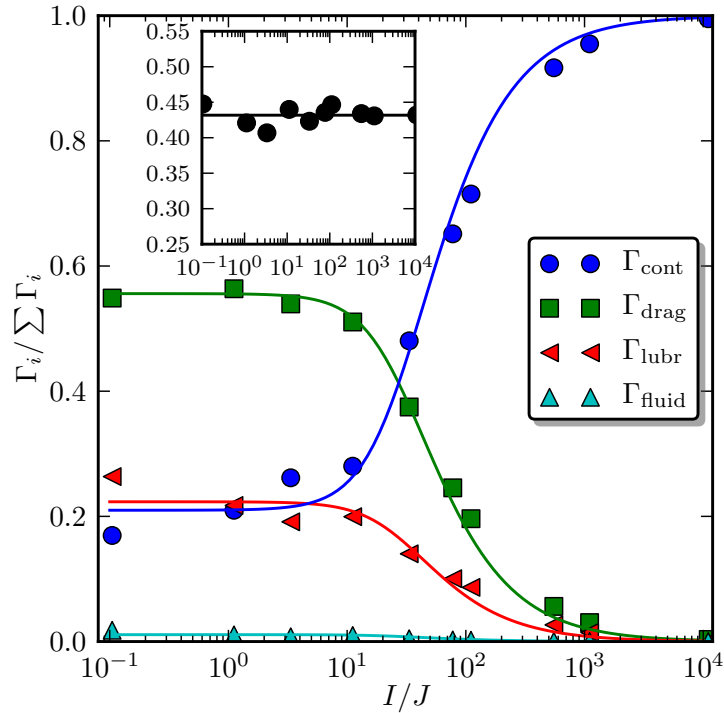


Boyer et al., PRL **107**, 188301 (2011).

$$J = \frac{\eta_f \dot{\gamma}}{P} \quad (I_v \equiv J)$$



Transition from viscous to inertial regime



Adding dissipation

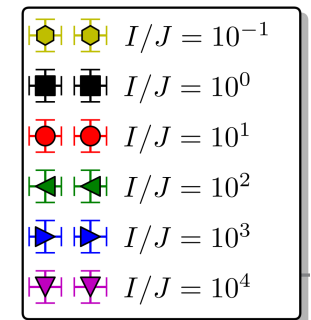
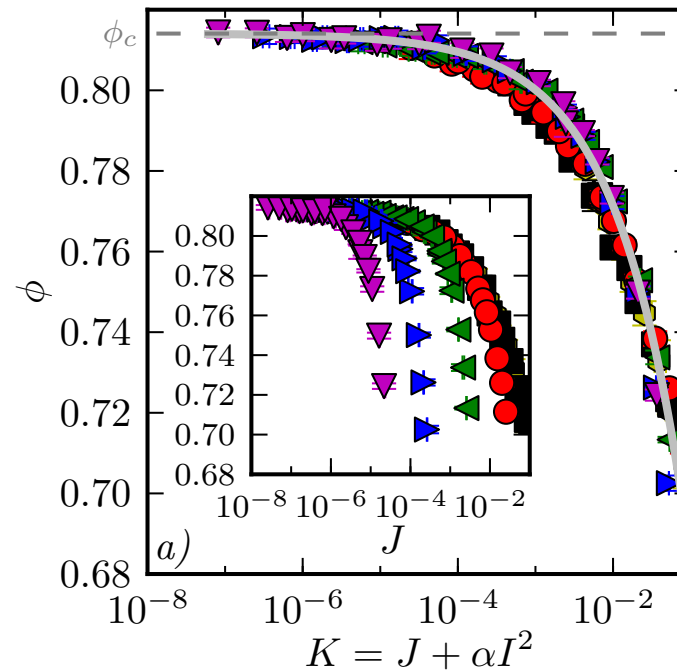
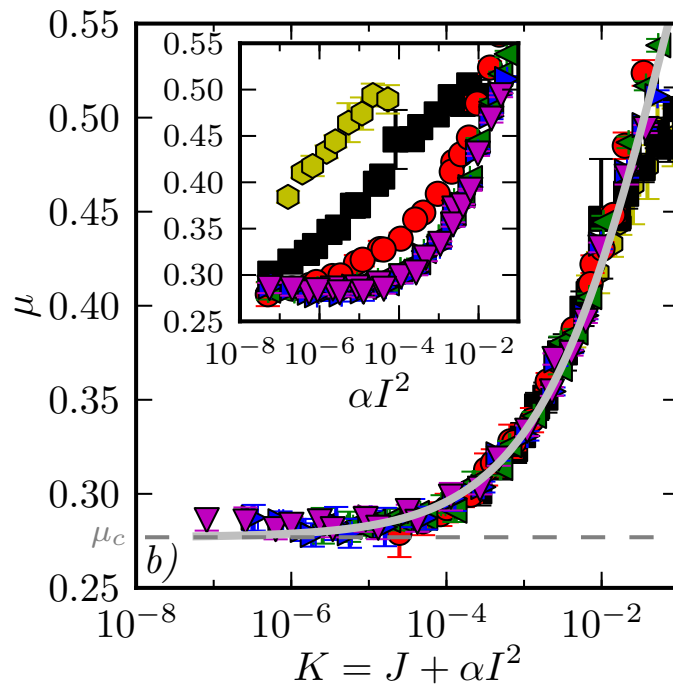
$$\tau = f_\tau(\phi) (\eta_f \dot{\gamma} + \alpha \rho d^2 \dot{\gamma}^2)$$

$$P = f_P(\phi) (\eta_f \dot{\gamma} + \alpha \rho d^2 \dot{\gamma}^2)$$

Stokes number

$$I^2 / J = \dot{\gamma} d^2 \rho / \eta_f \simeq 1 / \alpha$$

$$K = J + \alpha I^2$$



Brownian particles

Péclet number

$$\text{Pe} = \frac{\eta_f \dot{\gamma}}{k_B T / d^3}$$

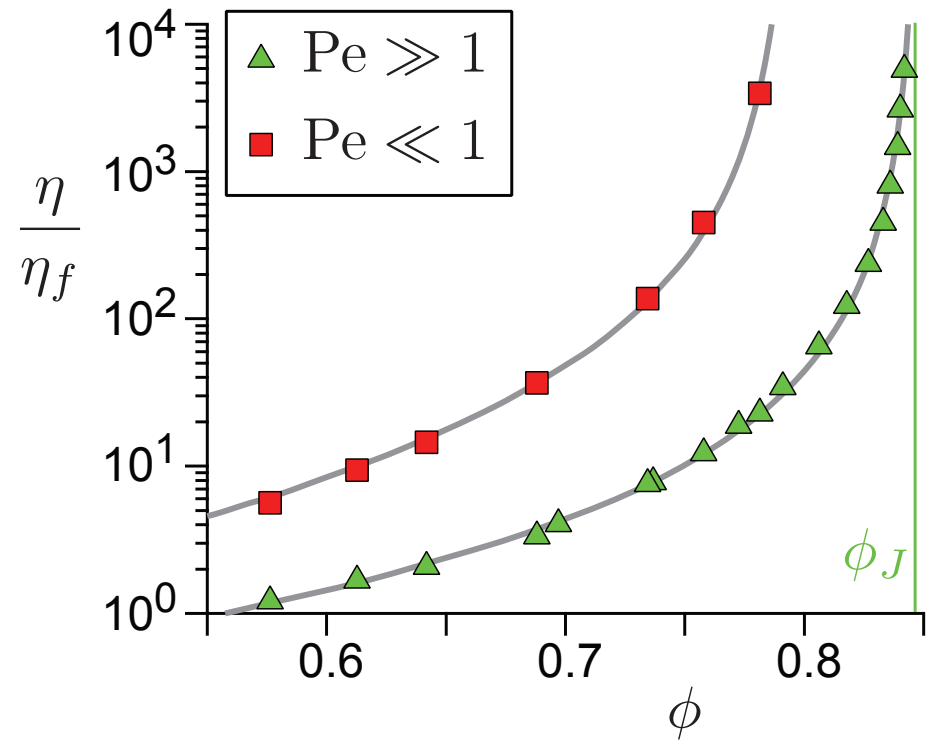
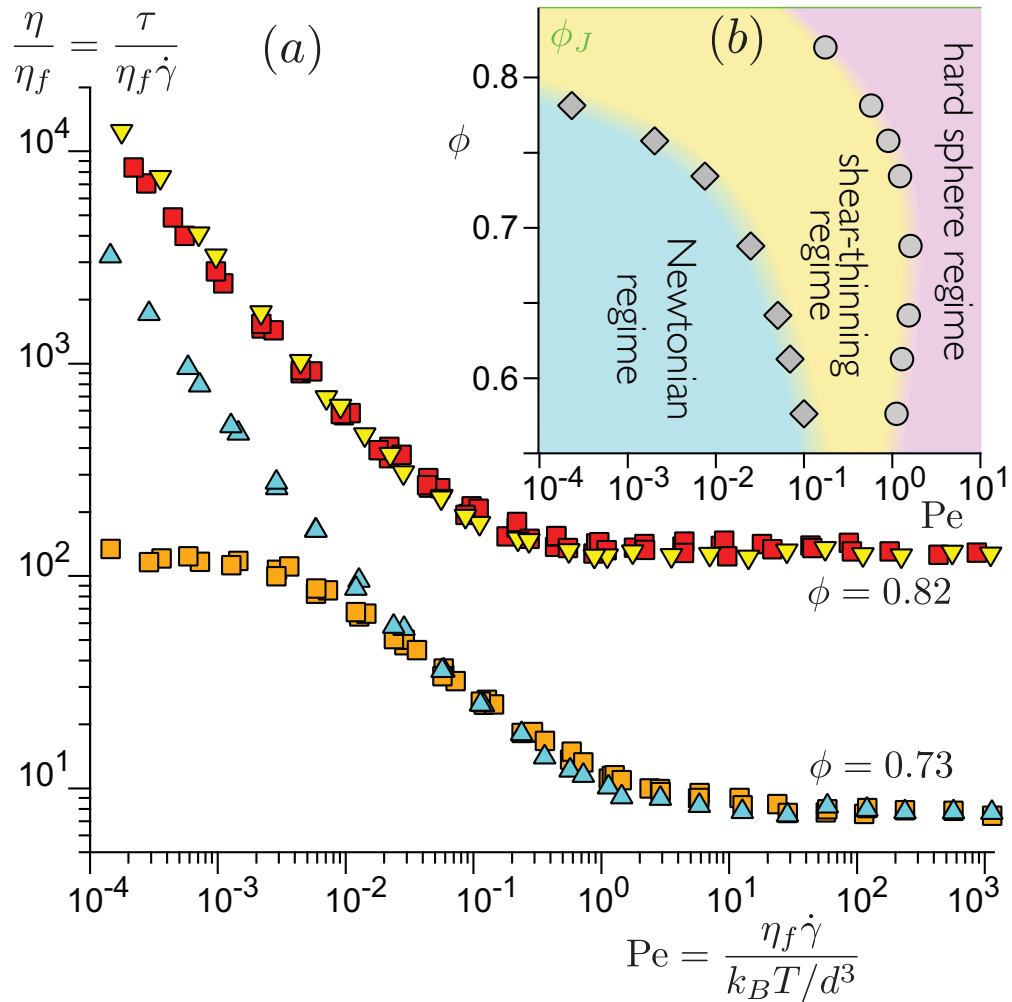
Overdamped Langevin equation

$$-\frac{3\pi\eta_f}{(1-\phi)}\delta\mathbf{u}_i + \sum_{j \neq i} \mathbf{f}_{ij} + \boldsymbol{\xi}_i = 0$$

$$\delta\mathbf{u}_i \equiv \mathbf{u}_i - \dot{\gamma} z \mathbf{e}_x$$

$$\langle \boldsymbol{\xi}_i(t) \boldsymbol{\xi}_j(t') \rangle = 6\pi\eta_f k_B T / (1-\phi) \delta_{ij} \delta(t-t')$$

Rheology



Athermal analogue

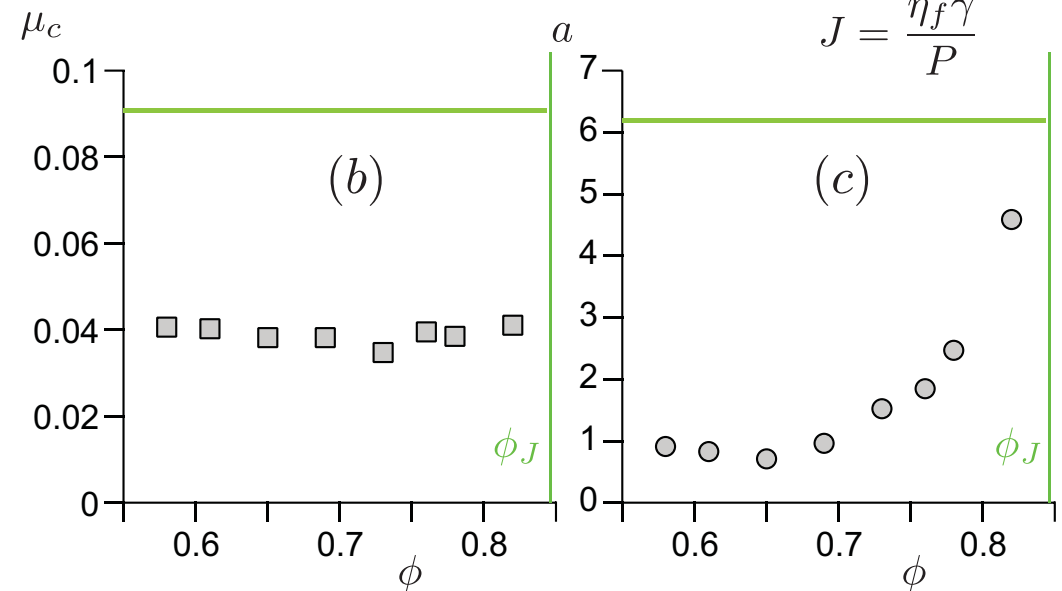
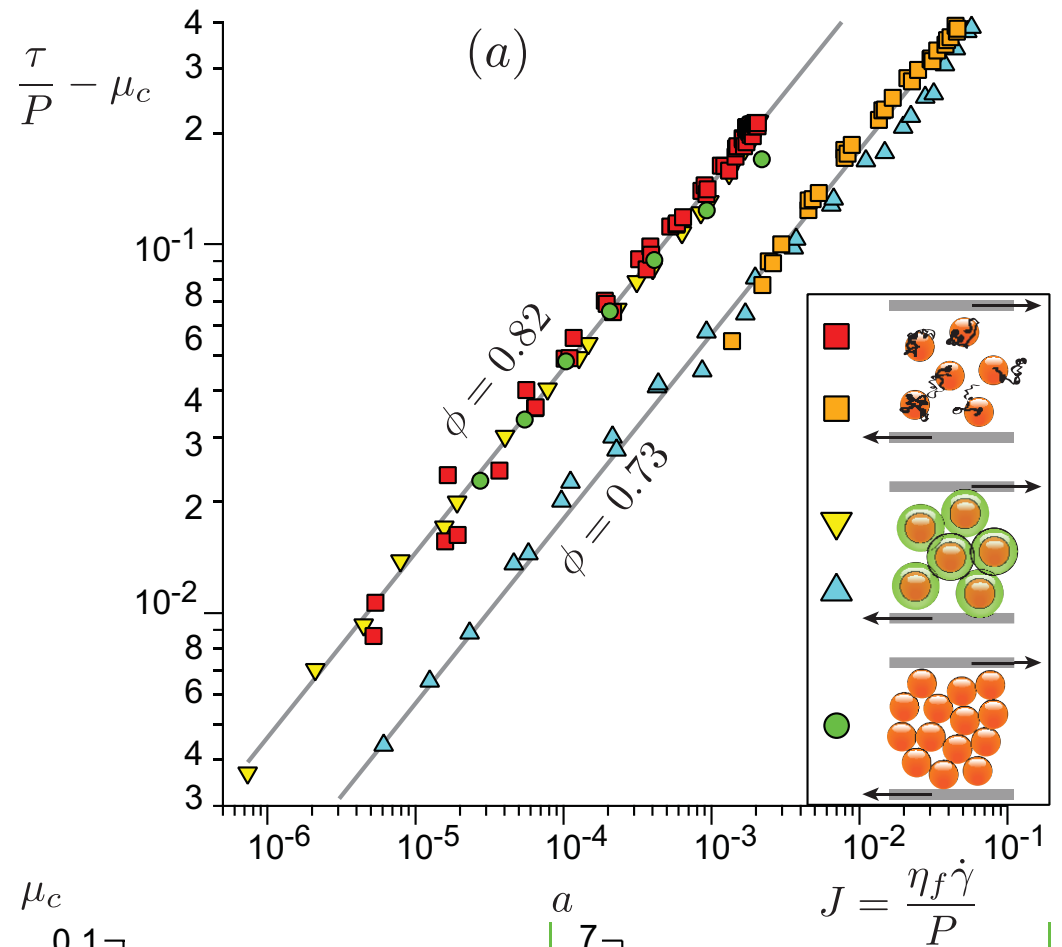
Effective potential

$$\varphi(r) = -k_B T \ln \frac{r-d}{d}$$

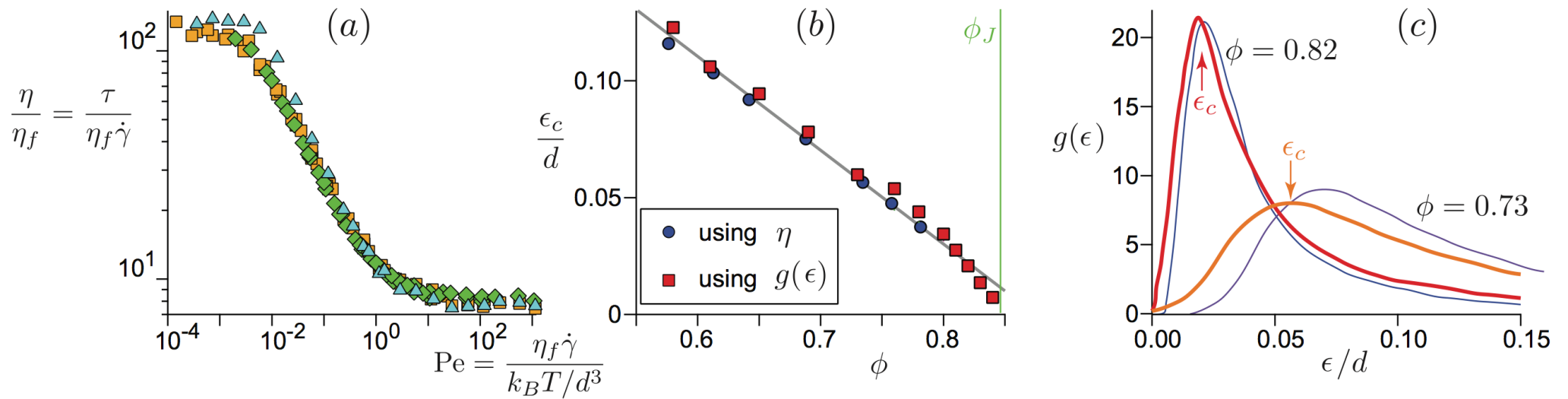
Brito & Wyart EPL **76**, 149 (2006).

Herschel-Bulkley rheology

$$\frac{\tau}{P} = \mu_c + aJ^{0.5}$$

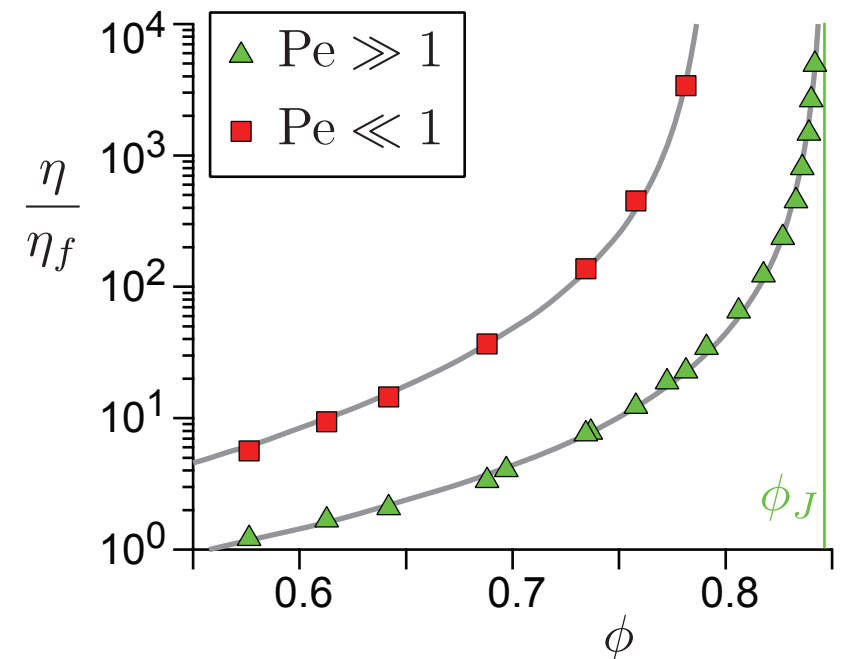


Phenomenological cut-off length



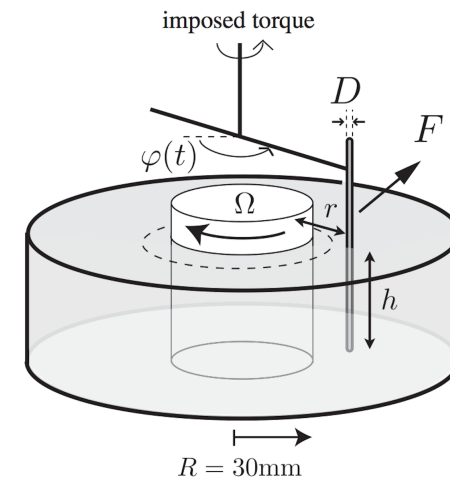
$$\eta_B(\phi) = \eta_H \left[\left(1 + \frac{\epsilon_c}{d} \right)^2 \phi \right]$$

■ ▲

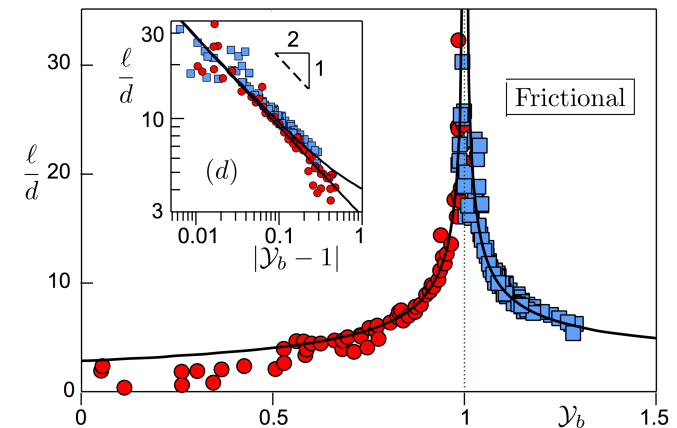


Beyond the local rheology

Reddy et al., PRL **106**,
108301 (2011).



$$\mathcal{Y}_b = \frac{\mu}{\mu_c} = \frac{\tau}{\mu_c P}$$



- Non-local effects
- Spatial relaxation length
- Non-local constitutive relations
Order parameter: fluidity f

$$\frac{\tau}{P} = \mu(I) [1 - \chi(\kappa)]$$

$$\kappa = \frac{d^2 \nabla^2 f}{f}$$

$$\chi(\kappa) = \nu \kappa + \mathcal{O}(\kappa^2)$$

$$f = I = \frac{|\dot{\gamma}| d}{\sqrt{P/\rho}}$$

Related publications

[1] *Transition from viscous to inertial regime in dense suspensions*

M. Trulsson, B. Andreotti and P. Claudin

Phys. Rev. Lett. **109**, 118305 (2012).

[2] *A non-local rheology for granular flows across yield conditions*

M. Bouzid, M. Trulsson, P. Claudin, E. Clément and B. Andreotti

Phys. Rev. Lett. **111**, 238301 (2013).

[3] *Dynamic compressibility of dense granular shear flows*

M. Trulsson, M. Bouzid, P. Claudin and B. Andreotti

Europhys. Lett. **103**, 38002 (2013).

[4] *Microrheology to probe non-local effects in dense granular flows*

M. Bouzid, M. Trulsson, P. Claudin, E. Clément and B. Andreotti

Europhys. Lett. **109**, 24002 (2015).

[5] *Athermal analogue of sheared dense Brownian suspensions*

M. Trulsson, M. Bouzid, J. Kurchan, E. Clément, P. Claudin and B. Andreotti

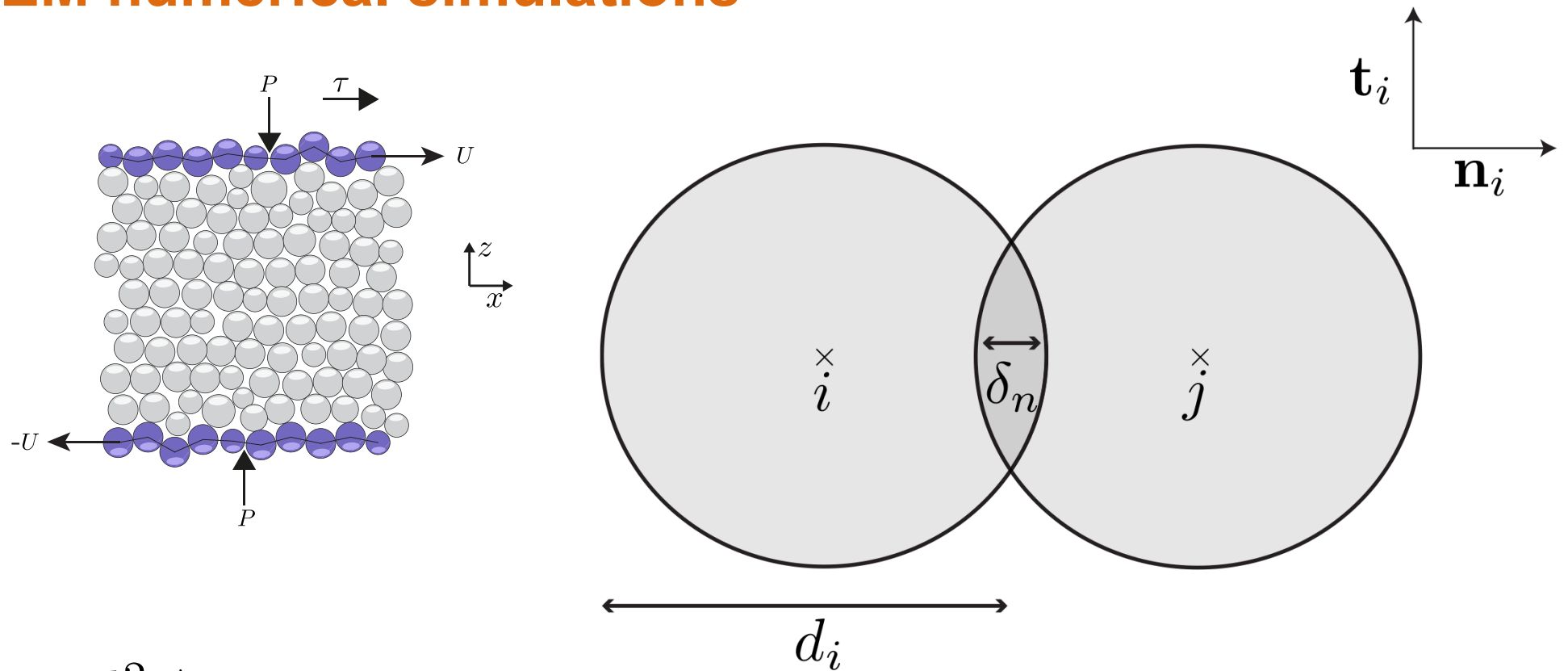
Europhys. Lett. **111**, 18001 (2015).

[6] *Non-local rheology in dense granular flows -- Revisiting the concept of fluidity*

M. Bouzid, A. Izzet, M. Trulsson, E. Clément, P. Claudin and B. Andreotti

Accepted EPJE.

DEM numerical simulations



$$m_i \frac{d^2 \vec{r}_i}{dt^2} = \sum_{j \neq i} \vec{F}_{ij} + \vec{F}_{\text{ext}}$$

$$I_i \frac{d\vec{\omega}_i}{dt} = \sum_{j \neq i} d_i \vec{n}_{ij} \times \vec{F}_{ij}$$

contact laws

$$\frac{k_n}{P}$$

Change of representation

$$\frac{\tau}{P} = \mu_c (1 + aI^n) \qquad I = \frac{\dot{\gamma}d}{\sqrt{P/\rho}}$$

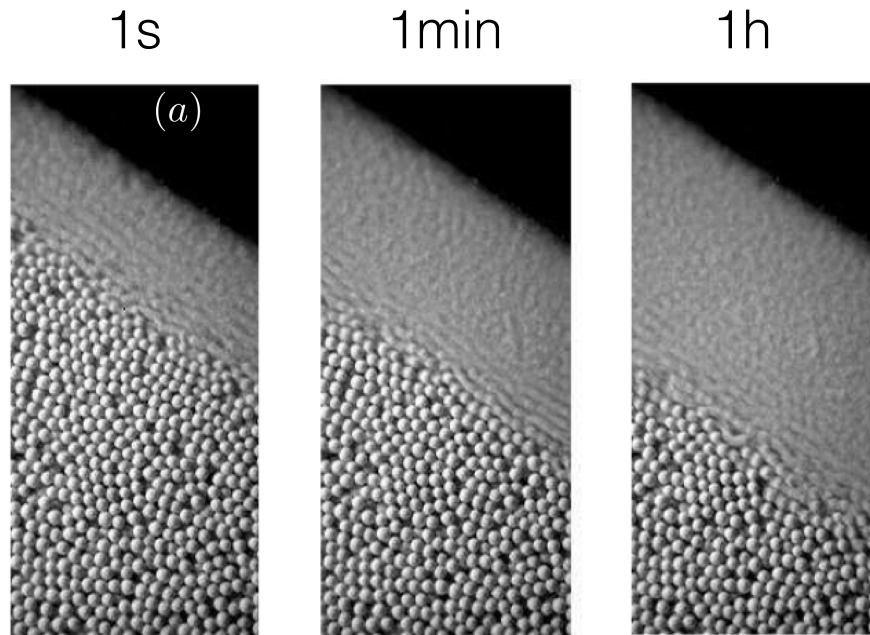
$$\phi = \phi_c - bI^n$$

$$P = b^{2/n} \frac{\rho \dot{\gamma}^2 d^2}{(\phi_c - \phi)^{2/n}}$$

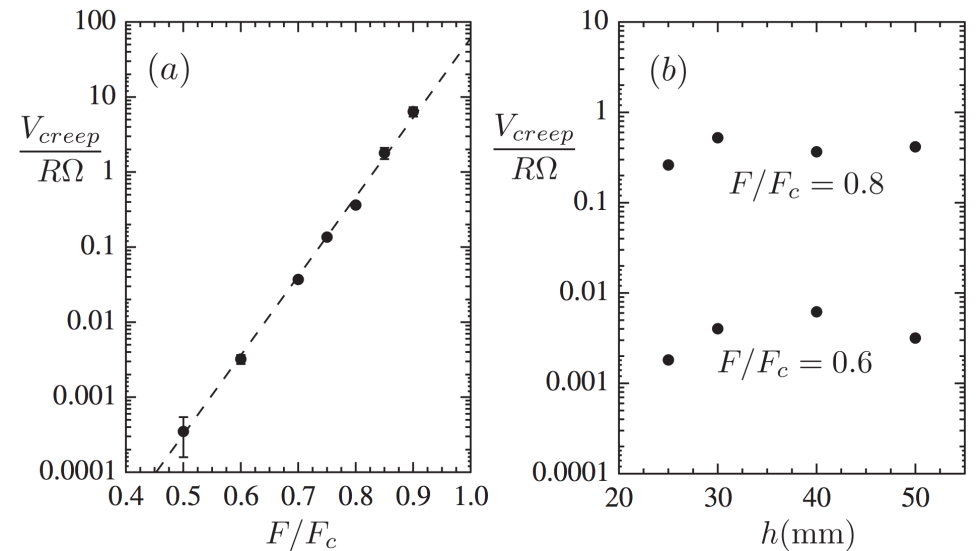
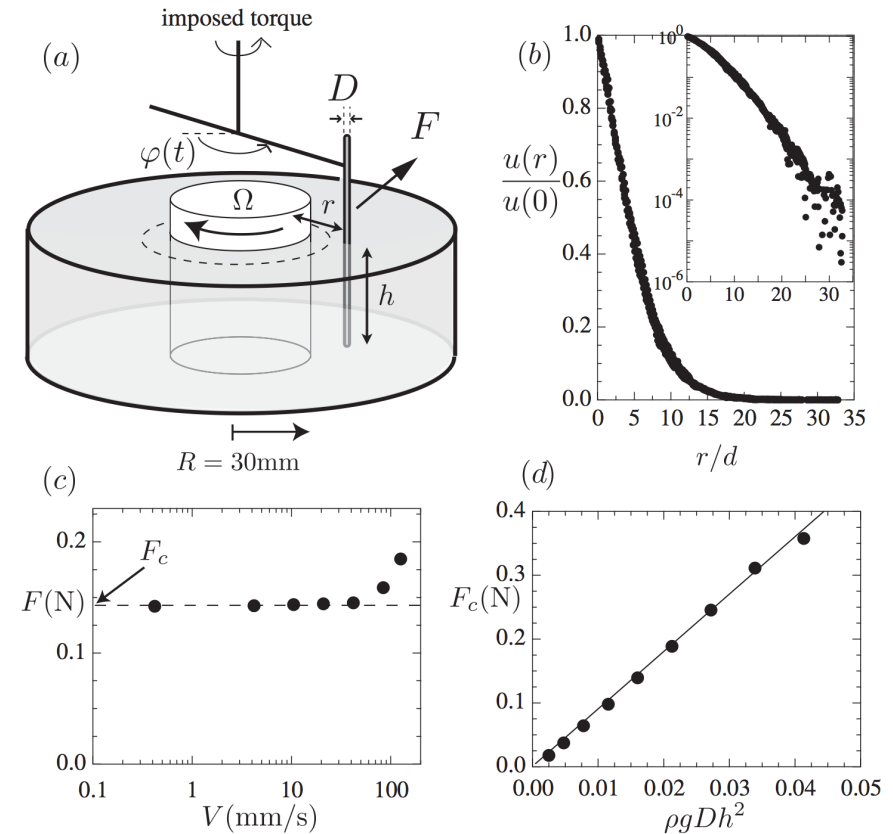
$$\tau = \mu_c b^{2/n} \left(1 + \frac{a}{b} (\phi_c - \phi) \right) \frac{\rho \dot{\gamma}^2 d^2}{(\phi_c - \phi)^{2/n}}$$

Non-Local flowing effects

Reddy et al., PRL **106**, 108301 (2011).



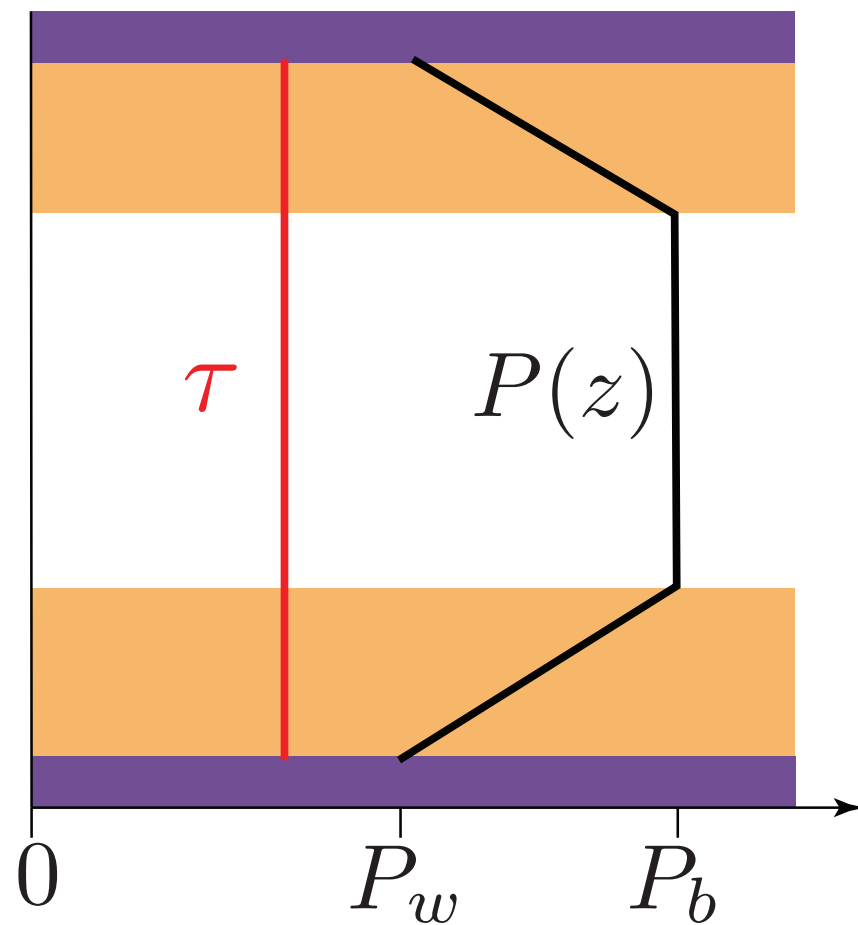
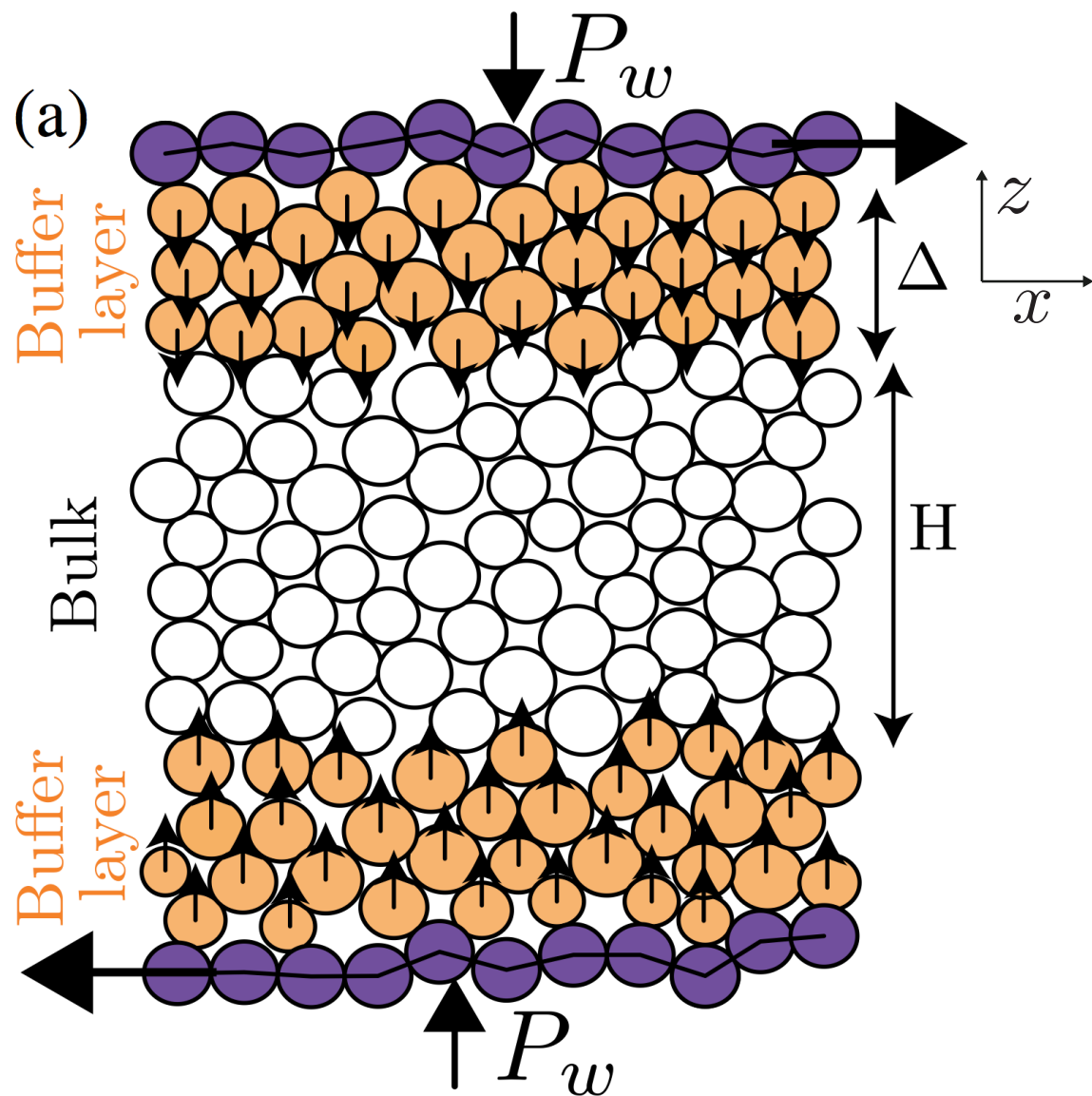
Komatsu et al., PRL **86**, 1757 (2001).



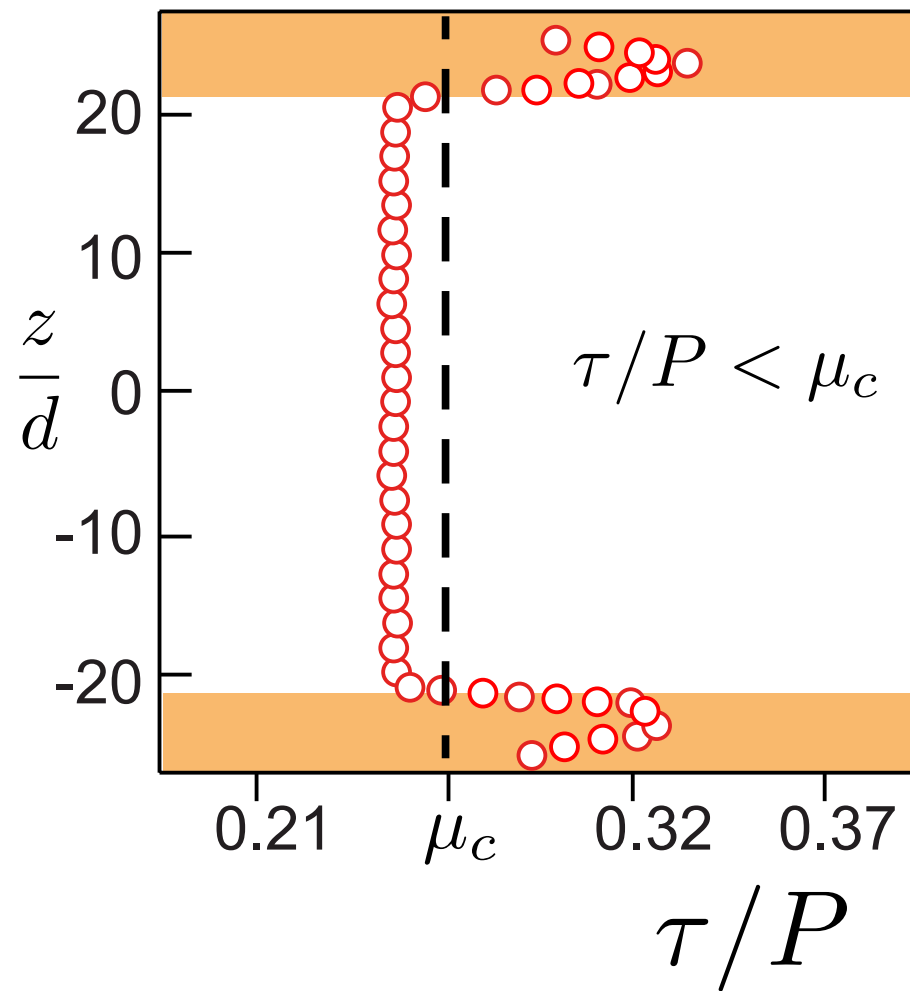
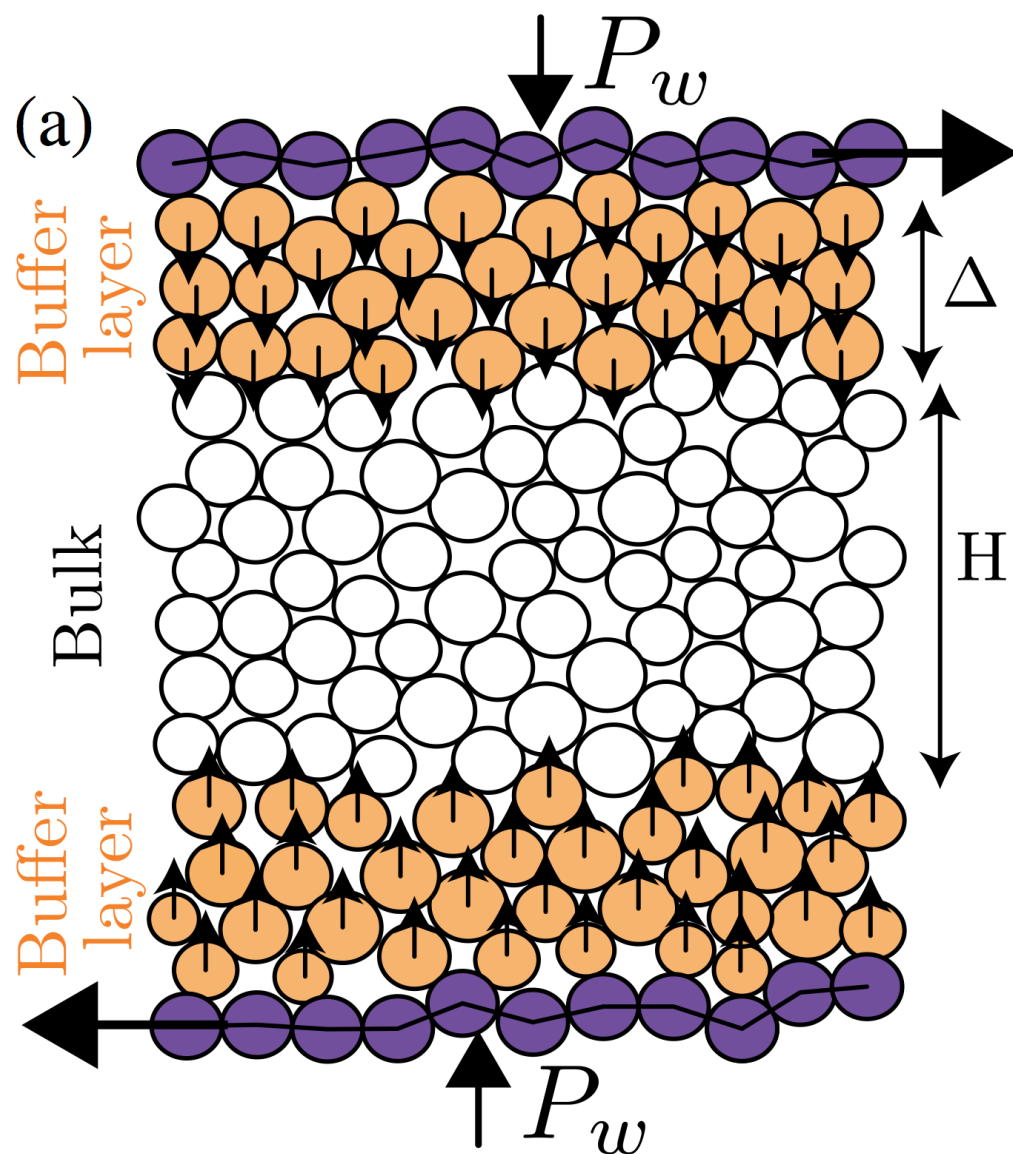
Goyon et al., Nature **454**, 84 (2008).

Nichol et al., PRL **104** 078302 (2010).

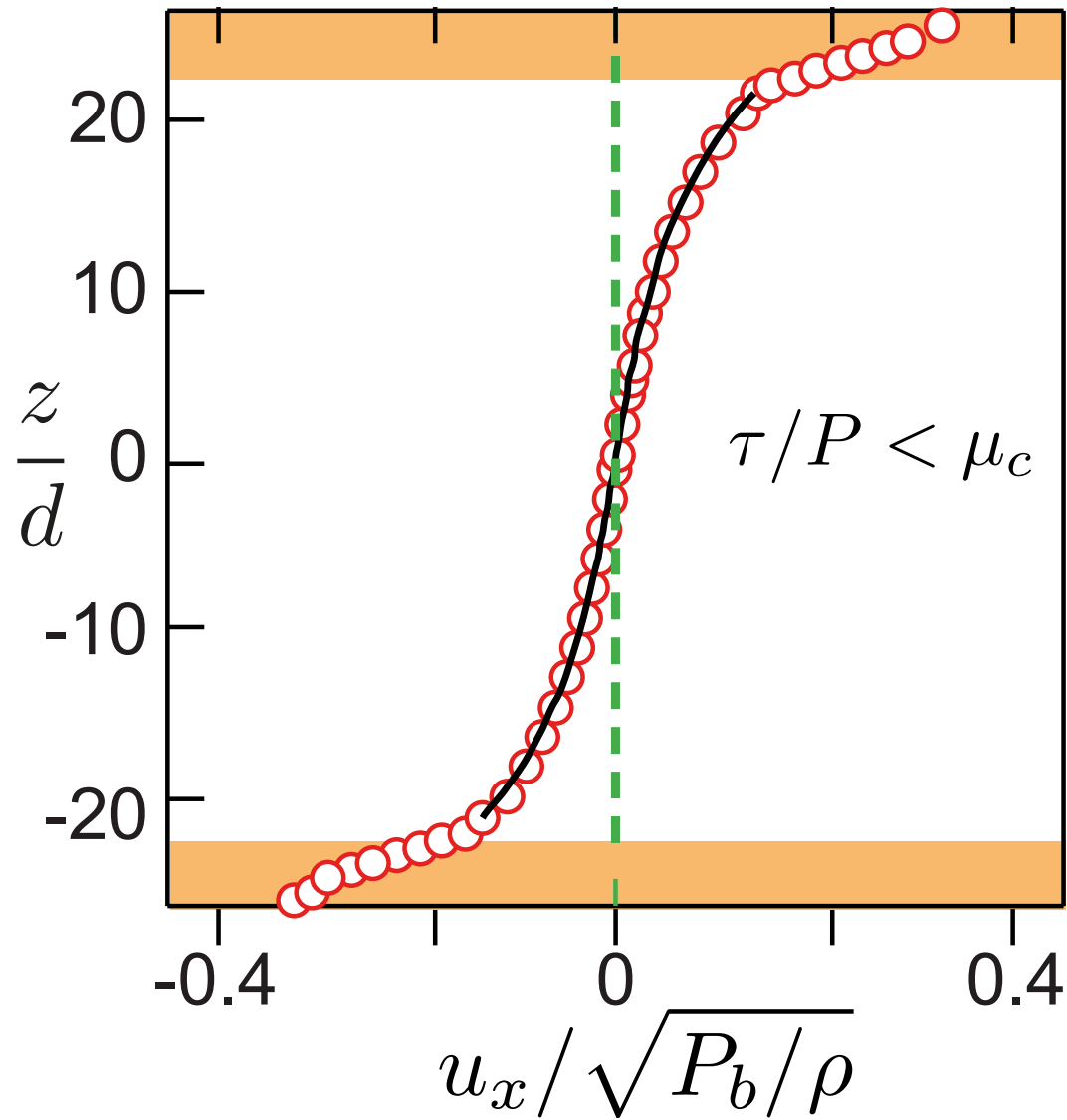
Numerical set-up



Can one create a solid/liquid interface?



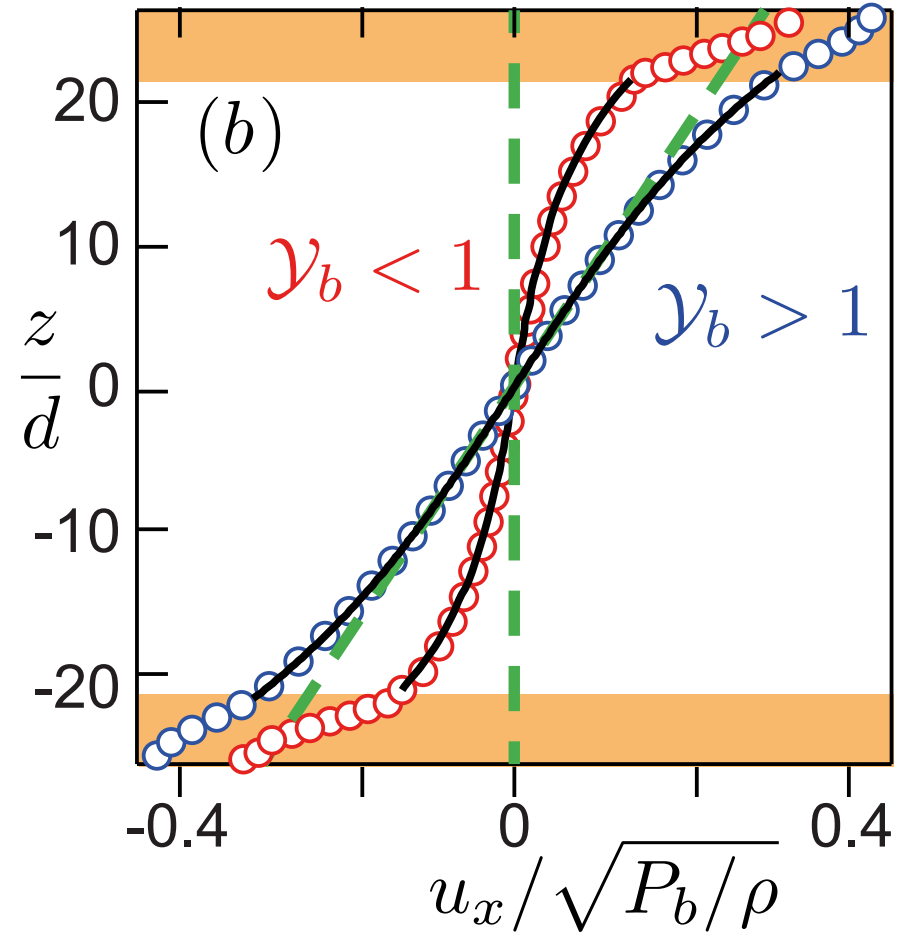
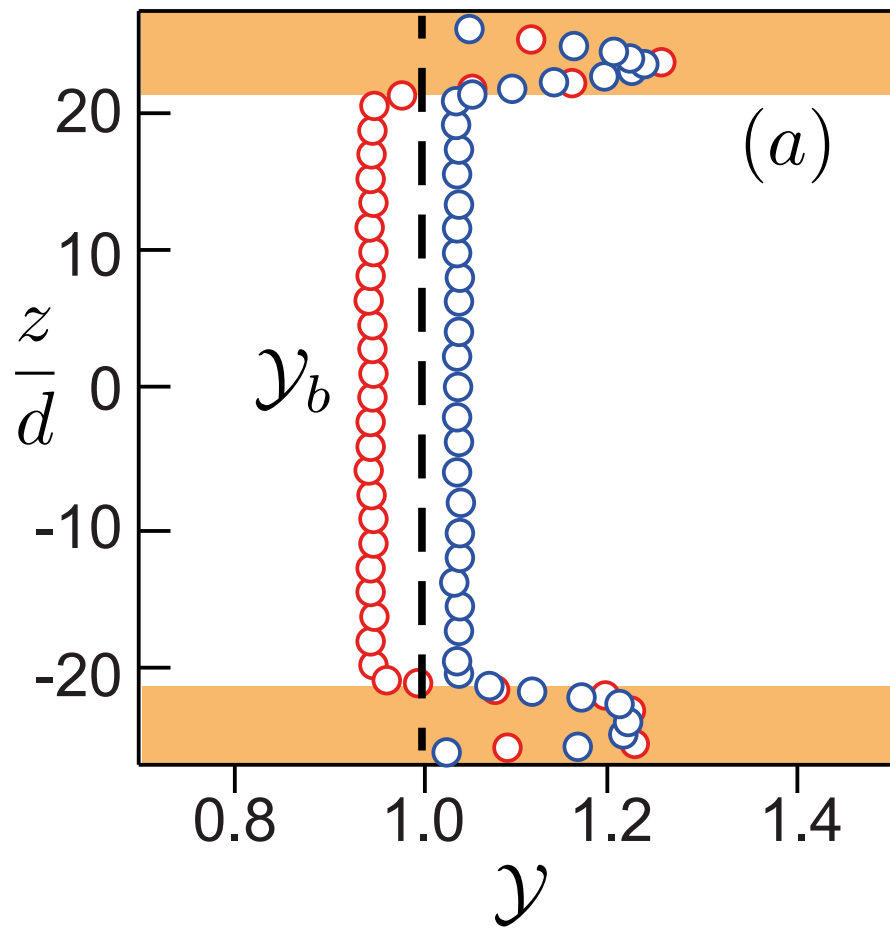
E pur si muove!



τ/P (or \mathcal{Y})
does not control the
solid/liquid transition

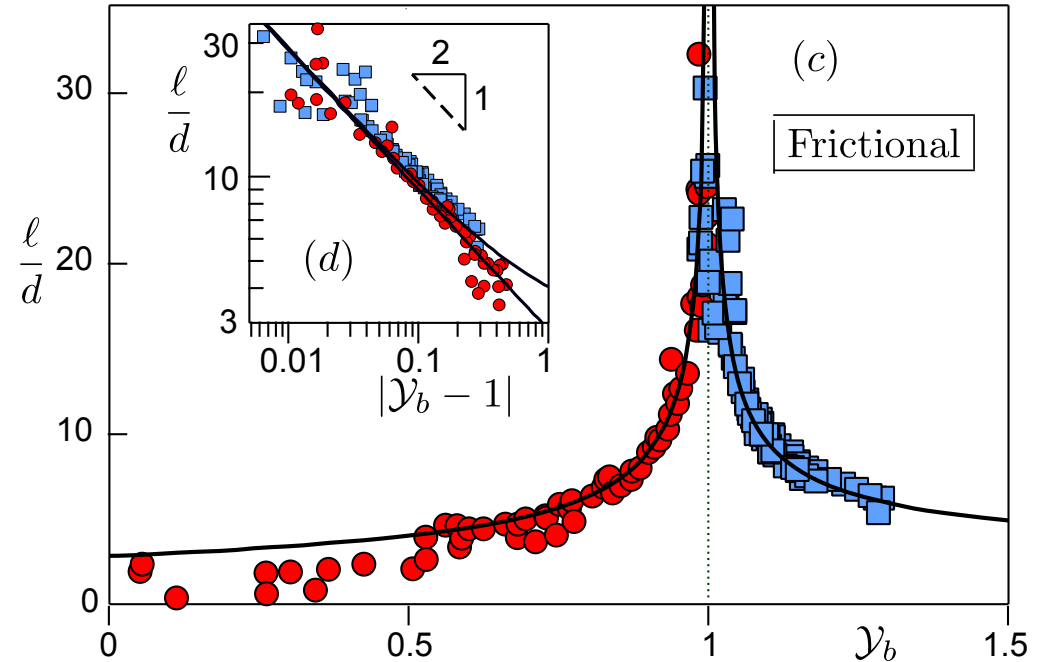
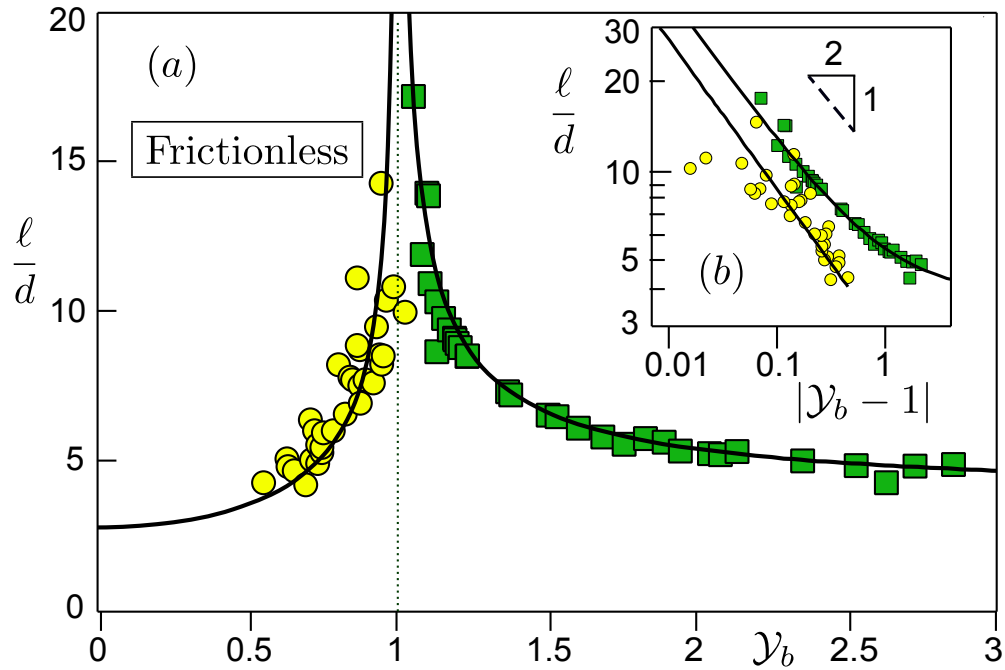
spatial relaxation
 $e^{\pm z/l}$

Relaxation length (1)



$$u_x(z) = \dot{\gamma}_\infty z + \frac{u_x(H/2) - \dot{\gamma}_\infty H/2}{\sinh(H/(2\ell))} \sinh(z/\ell)$$

Relaxation length (2)



A single liquid phase: the divergence is NOT the signature of change of state.

Fluidity

Order parameter: fluidity

Fluidity must depend on state variables only

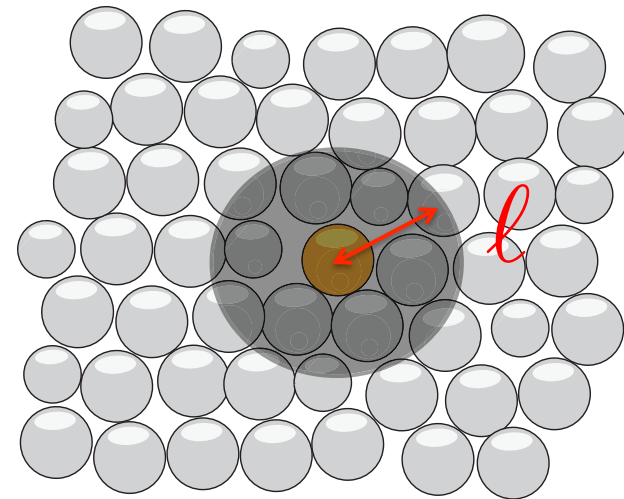
Relative environment fluidity

$$\kappa = \frac{d^2 \nabla^2 f}{f}$$

$f = 0$ solid

$f \neq 0$ liquid

I Z ϕ ~~χ~~



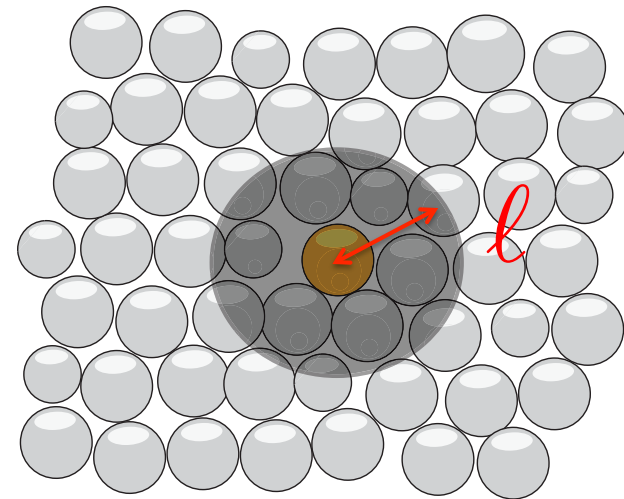
Non-local rheology

$$\frac{\tau}{P} = \mu(I) [1 - \chi(\kappa)]$$

$$\kappa = \frac{d^2 \nabla^2 f}{f}$$

$$\chi(\kappa) = \nu \kappa + \mathcal{O}(\kappa^2)$$

$$f = I = \frac{|\dot{\gamma}| d}{\sqrt{P/\rho}}$$



Linearisation

$$\mathcal{Y} = \frac{\mu(I)}{\mu_c} [1 - \nu\kappa]$$

$$\mu = \mu_c + aI^\alpha$$

$$\kappa \equiv d^2 \frac{\nabla^2 I}{I}$$

$$\mathcal{Y}_b > 1$$

$$I = I_b + \delta I$$

$$\ell^2 \frac{d^2 \delta I}{dz^2} - \delta I = 0$$

$$\ell_{>} = d \sqrt{\frac{\mathcal{Y}_b \nu}{\alpha(\mathcal{Y}_b - 1)}}$$

$$\mathcal{Y}_b < 1$$

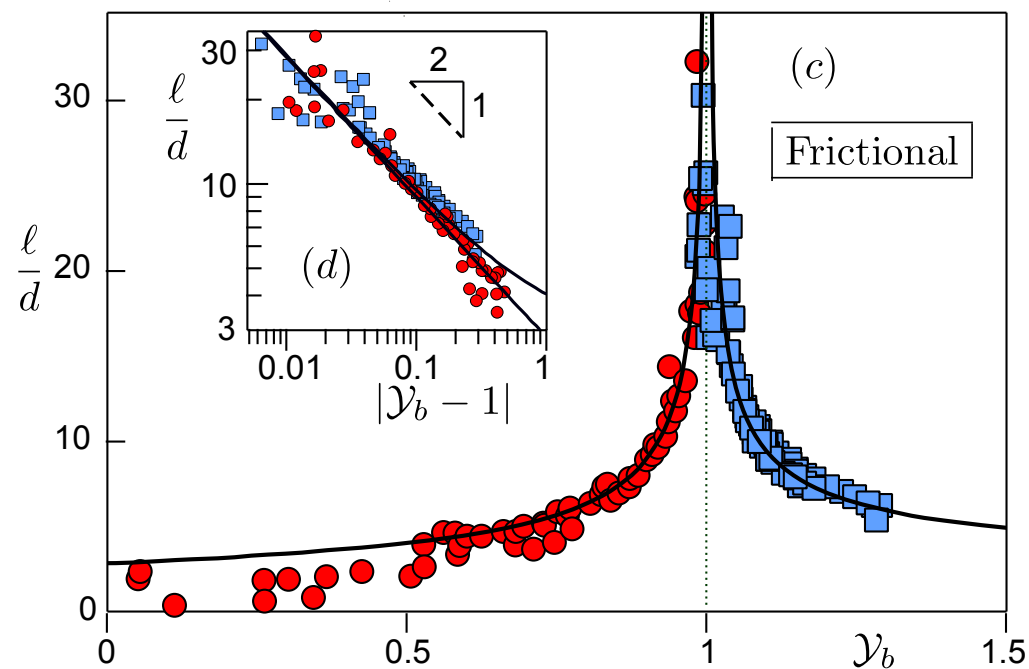
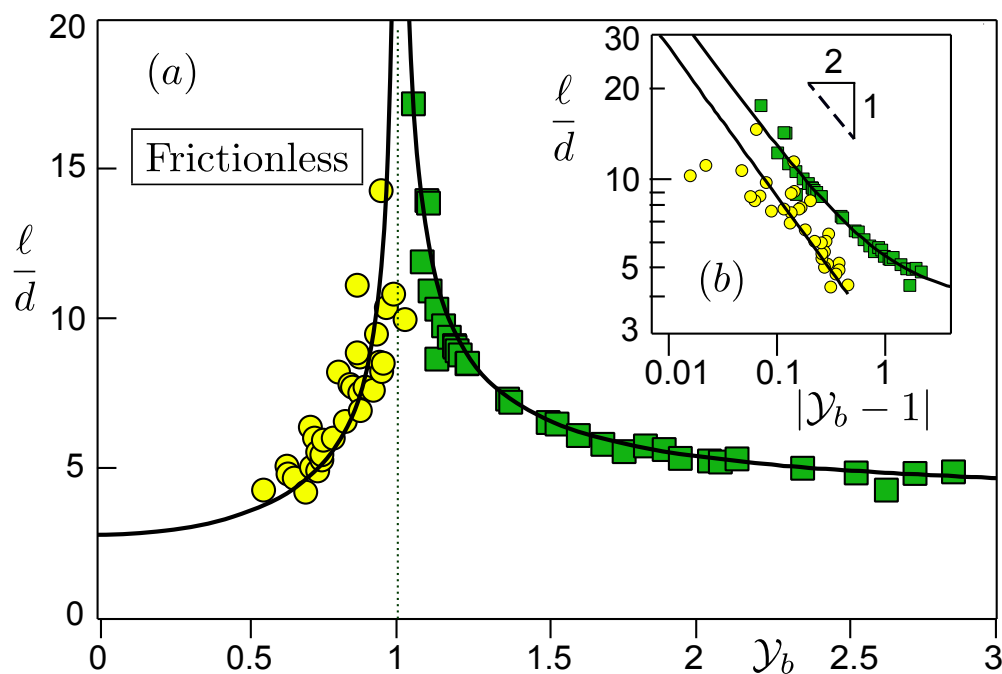
$$I = \delta I \quad (I_b = 0)$$

$$\kappa = (1 - \mathcal{Y}_b)/\nu$$

$$\ell^2 \frac{d^2 \delta I}{dz^2} - \delta I = 0$$

$$\ell_{<} = d \sqrt{\frac{\nu}{\mathcal{Y}_b - 1}}$$

Relaxation length (3)



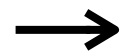
$$\ell_{>} = d \sqrt{\frac{\gamma_b \nu}{\alpha(\gamma_b - 1)}}$$

$$\ell_{<} = d \sqrt{\frac{\nu}{\gamma_b - 1}}$$

$$\nu \simeq 8$$

Some other approaches

- Phase field Aranson & Tsimring, PRE **64**, 1757 (2001).
- Mechanically activated plastic events Pouliquen & Forterre,
Phil. Trans. R. Soc. A. **367**, 5091 (2009).
- Kinetic elasto-plastic Bocquet et al., PRL **103**, 036001 (2009).
Kamrin & Koval, PRL **108**, 178301 (2012).

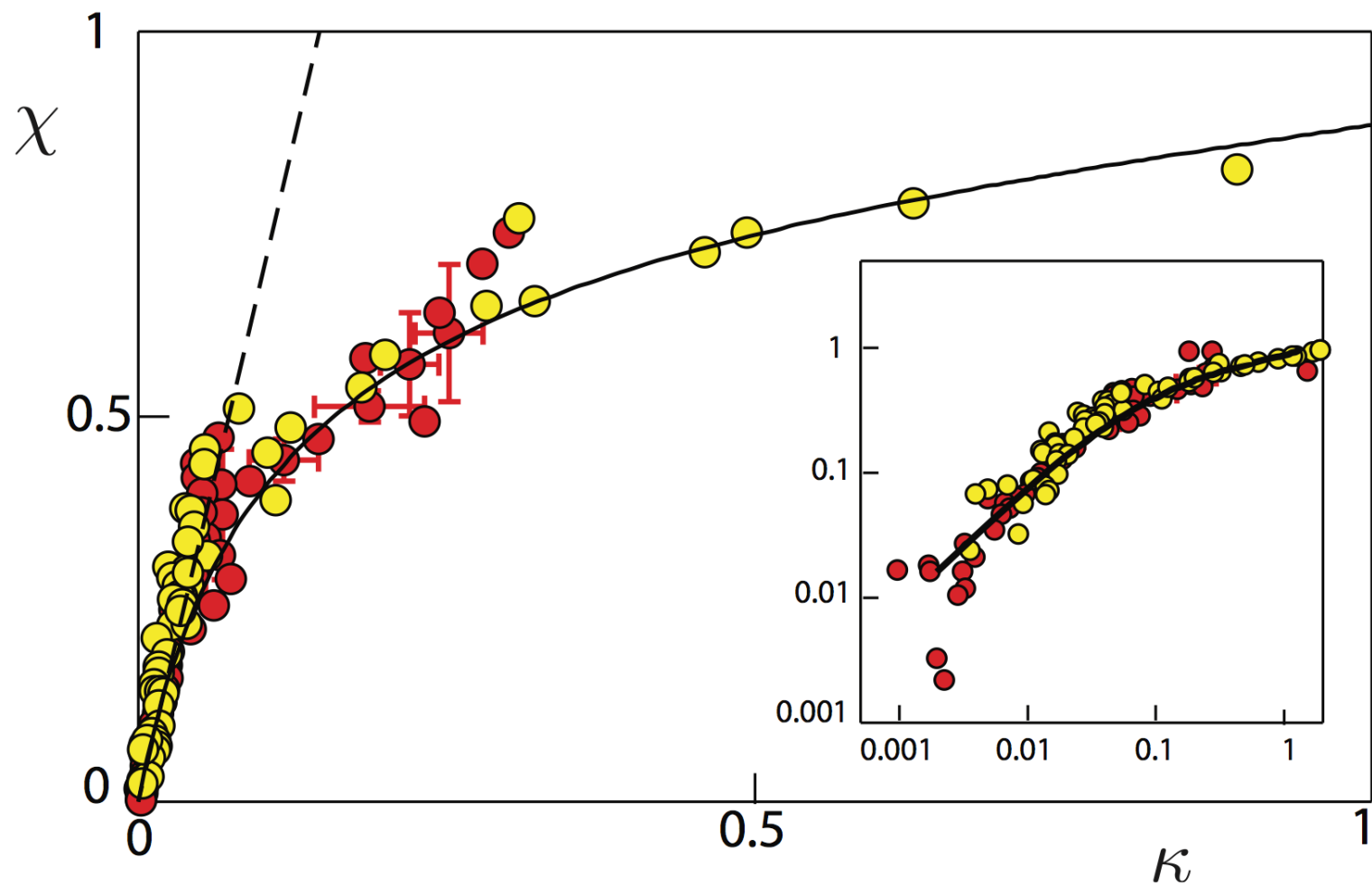


Choice for fluidity

Continuity and boundary conditions

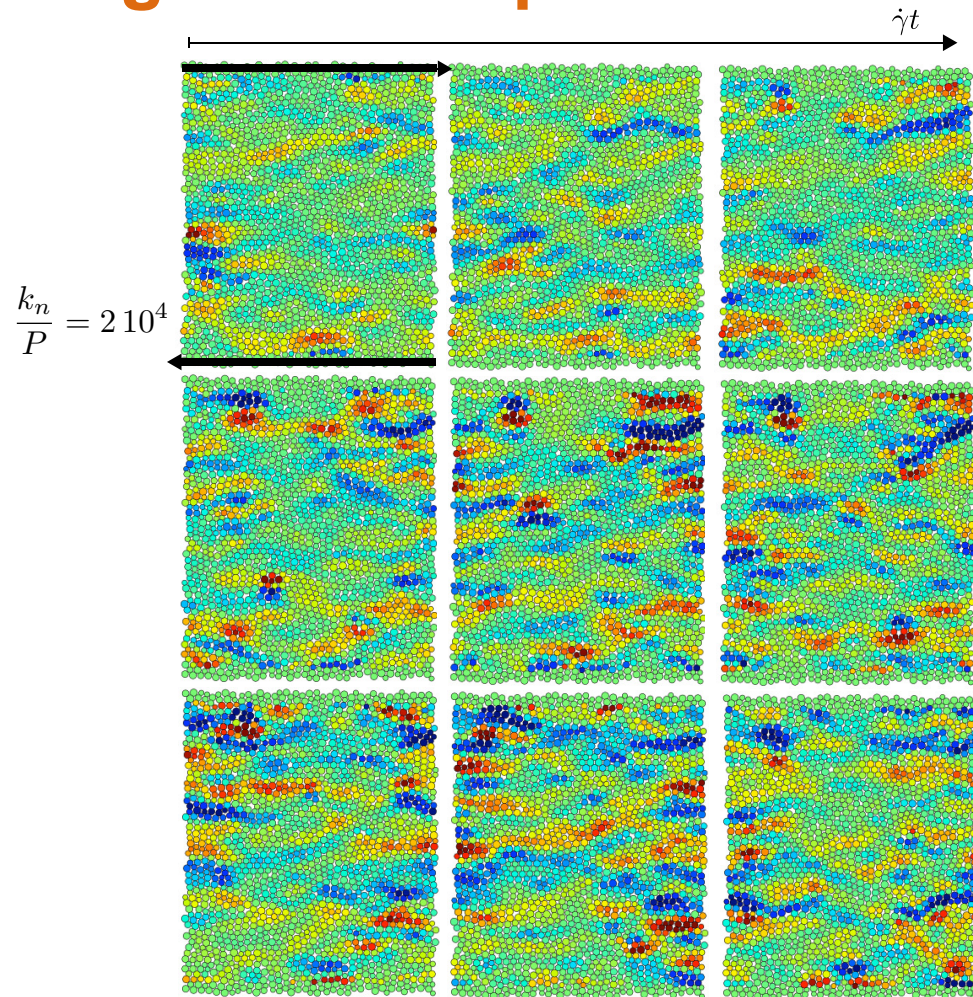
Assumptions and mechanisms

Non-linear non-local function

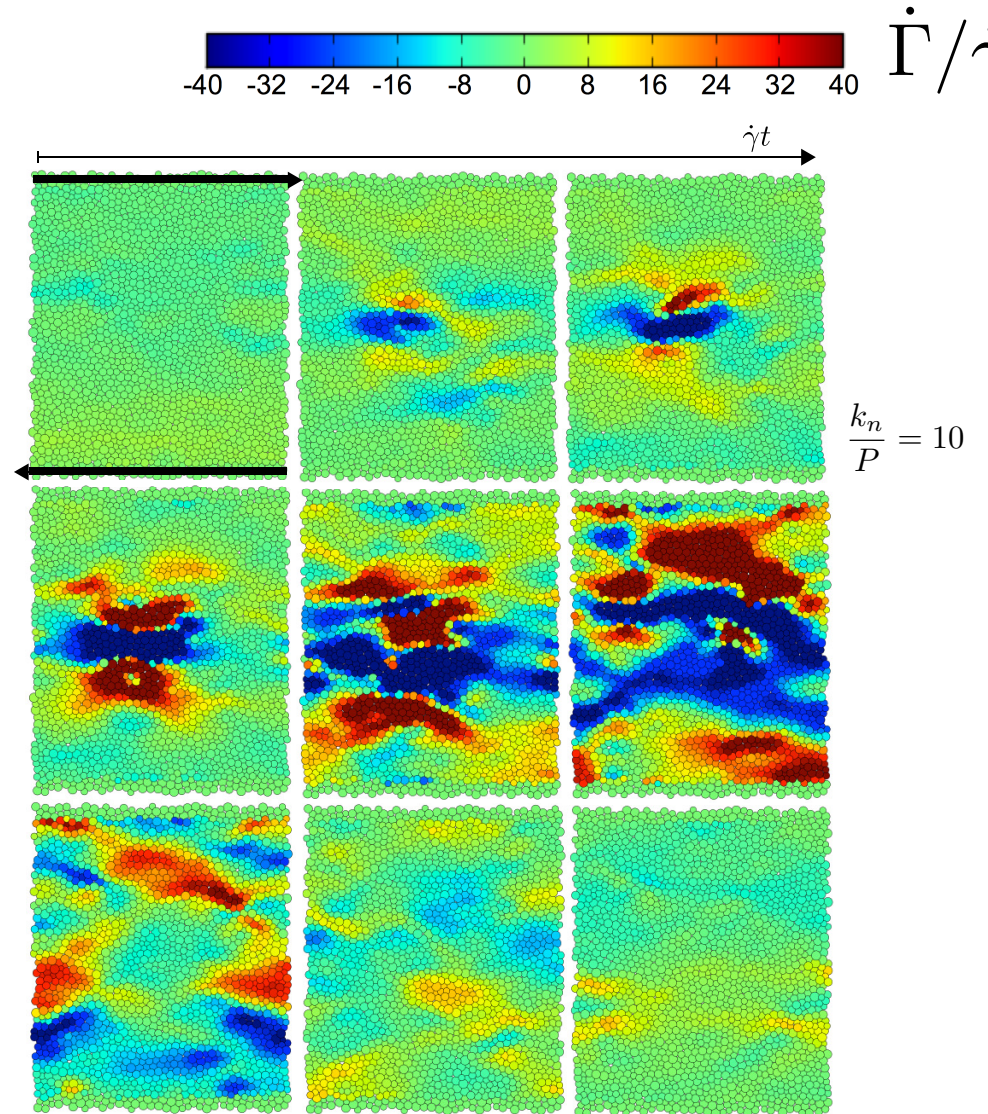


At linear order $\chi(\kappa) = \nu\kappa + \mathcal{O}(\kappa^2)$ with $\nu \simeq 8$

Rigid vs soft particles



No localized plastic events
Permanent spatial heterogeneities



Localized plastic events
Very intermittent dynamics

Local contribution of a region
to the mean shear rate $\dot{\gamma}$:

$$\dot{\Gamma}(\vec{r}, t) = \frac{\sum_{j=1}^N [u_i(\vec{r}, t) - u_j(\vec{r}, t)][z_i(t) - z_j(t)] \exp\left(\frac{-\|\Delta\vec{r}\|^2}{2\delta^2}\right)}{\sum_{j=1}^N [z_i(t) - z_j(t)]^2 \exp\left(\frac{-\|\Delta\vec{r}\|^2}{2\delta^2}\right)}$$

Rigid vs soft particles

